

IN THE CLAIMS

Please amend claim 48 as follows:

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~~48.~~ A method for suppressing formation of at least one undesirable chemical reaction product in a thermal chemical reaction, comprising:

- passing at least one reactant into at least one reaction chamber;
- said reaction chamber comprising a porous catalyst that catalyzes the reaction of said at least one reactant;
- transferring heat to or from said at least one reaction chamber from or into at least one heat exchanger;
- obtaining at least one product from said reaction chamber;
- at steady-state, transferring at least 0.6 W of heat per cc of total reactor volume, such that, at steady state, the catalyst is maintained within a temperature range that reduces the formation of at least one undesirable chemical reaction product; and
- maintaining a contact time of the reactant at less than 0.01 seconds, thereby suppressing slow reactions and reducing the formation of at least one undesirable chemical reaction products;

wherein said porous catalyst comprises a metal support.

Please add new claims 49-71 as follows:

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~~49.~~ The process of claim 1 wherein the catalyst comprises a monolith having a thickness of about 1 to about 3 mm.

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~~50.~~ The process of claim 1 wherein the reaction chamber has a length less than or equal to 6 inches and a height less than or equal to 2 inches.

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~~51.~~ The process of claim ~~50~~¹¹ which is conducted in parallel in multiple reaction chambers, wherein each of the reaction chambers has a height less than 2 cm.

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~~52.~~ The process of claim ~~2~~¹ wherein the process produces less than about 0.5

SLPM of hydrogen gas per cubic centimeter of reactor volume.

~~15~~ 53. The process of claim ~~14~~ 52 wherein the reaction chamber has a length less than or equal to 6 inches and a height less than or equal to 2 inches.

~~16~~ 54. The process of claim ~~15~~ 53 wherein the heat exchanger comprises a fluid selected from the group consisting of: a combustion stream, steam and oil.

~~17~~ 55. The process of claim ~~16~~ 54 wherein the at least one heat exchanger has a thickness of 250 μ m to 3 mm.

~~18~~ 56. The process of claim ~~15~~ 53 wherein the pressure drop through the reaction chamber is less than 10 psig.

~~24~~ 57. The process of claim ~~19~~ 56 wherein the reaction chamber has a length less than or equal to 6 inches and a height less than or equal to 2 inches.

~~25~~ 58. The process of claim ~~24~~ 57 which is conducted in parallel in multiple reaction chambers, wherein each of the reaction chambers has a height less than 2 cm.

~~26~~ 59. The process of claim ~~20~~ 57 which is conducted in parallel in multiple reaction chambers, wherein each of the reaction chambers has a height less than 2 cm.

~~27~~ 60. The process of claim ~~20~~ 57 wherein the reaction chamber has a length less than or equal to 6 inches and a height less than or equal to 2 inches.

~~28~~ 61. The process of claim ~~20~~ 57 wherein the at least one heat exchanger has a dimension of 250 μ m to 3 mm.

62. The apparatus of claim 10 wherein the at least one heat exchanger has a dimension of 250 μ m to 3 mm.

~~29~~ 63. The method of claim ~~29~~ 11 wherein the reaction chamber has a height in the range of 1 mm to 5 mm.

~~13~~ 64. The method of claim ~~12~~ 51 wherein the at least reaction chamber and the at least one heat exchanger are separated by a web having a thickness of between 0.01 and 0.25 inches.

65. The method of claim 2 wherein the at least reaction chamber and the at least one heat exchanger are separated by a web having a thickness of between 0.01 and 0.25 inches.

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86. The process of claim 14 wherein the at least reaction chamber and the at least one heat exchanger are separated by a web having a thickness of between 0.01 and 0.25 inches.

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87. The process of claim 28 which is conducted in parallel in multiple reaction chambers, wherein each of the reaction chambers has a height less than 2 cm.

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68. The process of claim 51 wherein the catalyst occupies at least 80% of the cross-sectional area of the reaction chamber.

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69. The process of claim 51 wherein the at least one heat exchanger has a thickness of 250 μ m to 3 mm.

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70. The method of claim 52 wherein the at least one heat exchanger has a thickness of 250 μ m to 3 mm.

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71. The method of claim 48 which is conducted in parallel in multiple reaction chambers, wherein each of the reaction chambers has a height less than 2 cm.